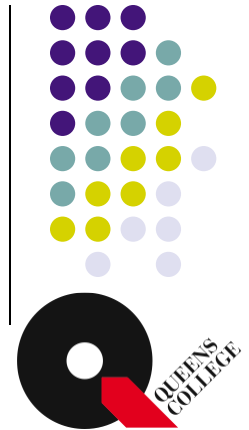


Chap. 3. The Second Law

↗ Law of Spontaneity, world gets more random

Kelvin - No process can transform heat completely into work



Chap. 3. The Second Law

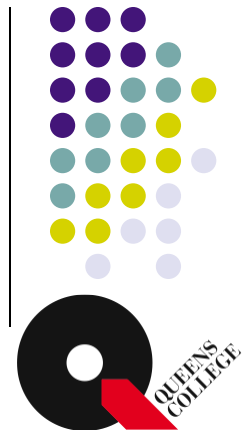
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The entropy of an isolated system increases in the course of a spontaneous change.

S - Entropy, the degree of randomness

- **State function, completely specified by thermodynamic variables**
- **Unit: Energy/temperature (K)**
- **Thermodynamic definition:** $TdS = dq_{rev}$



Chap. 3. The Second Law

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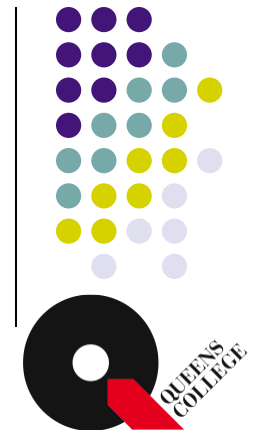
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The entropy of an isolated system increases in the course of a spontaneous change.

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- **Thermodynamic definition:** $TdS = dq_{rev}$

$$\Delta S = S_f - S_i = \int_i^f \frac{dq_{rev}}{T}$$

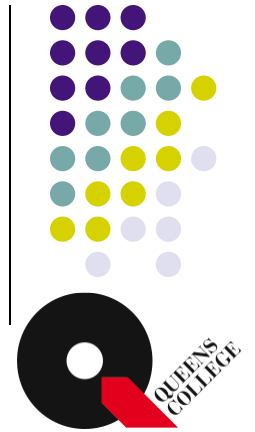


For surroundings, $dS_{sur} = \frac{dq_{sur}}{T_{sur}}$

because $dq_{sur} = dq_{sur,rev}$

**The above relation holds
even for finite amount of
heat**

$\longrightarrow \Delta S_{sur} = \frac{q_{sur}}{T_{sur}}$



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For adiabatic process, $\Delta S_{ad} = 0$



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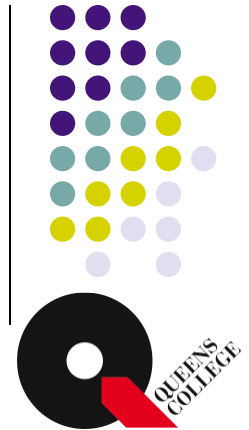
For adiabatic process, $\Delta S_{ad} = 0$

Isothermal expansion of an ideal gas

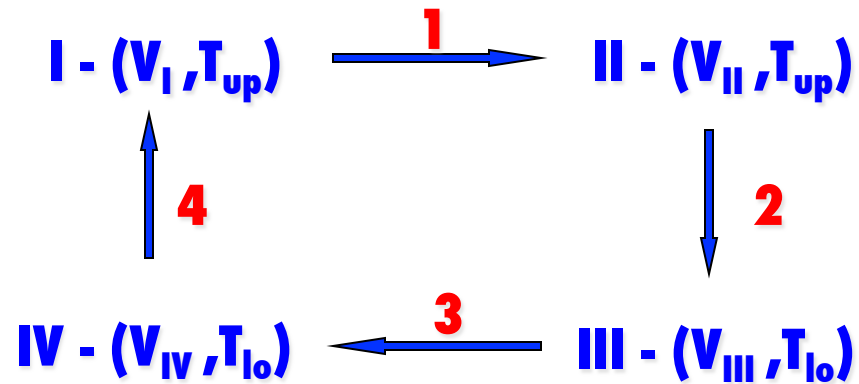
$$dU = 0 = dq_{rev} - pdV \longrightarrow dq_{rev} = pdV = \frac{nRT}{V}dV$$

$$\longrightarrow dS = \frac{dq_{rev}}{T} = \frac{nR}{V}dV$$

$$\longrightarrow \Delta S = \int_{V_i}^{V_f} dS = nR \int_{V_i}^{V_f} \frac{1}{V}dV = nR \ln \left(\frac{V_f}{V_i} \right)$$



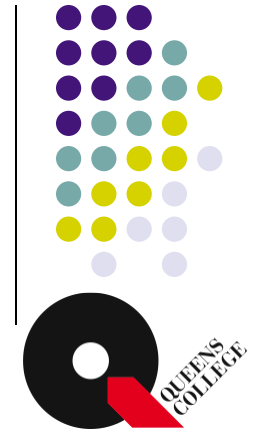
Carnot Cycle (Ideal Gas)



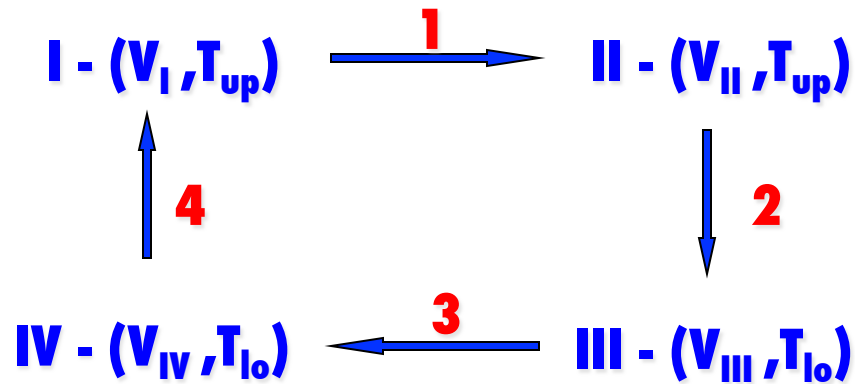
**Fig. 3.6 (with
different notations)**

1,3 - Reversible and isothermal processes

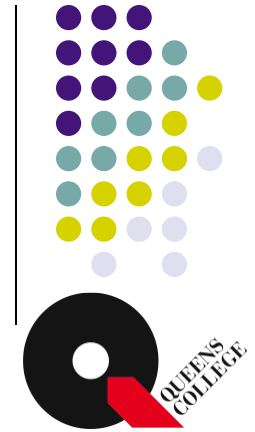
2,4 - Reversible and adiabatic processes



Carnot Cycle (Ideal Gas)



**Fig. 3.6 (with
different notations)**



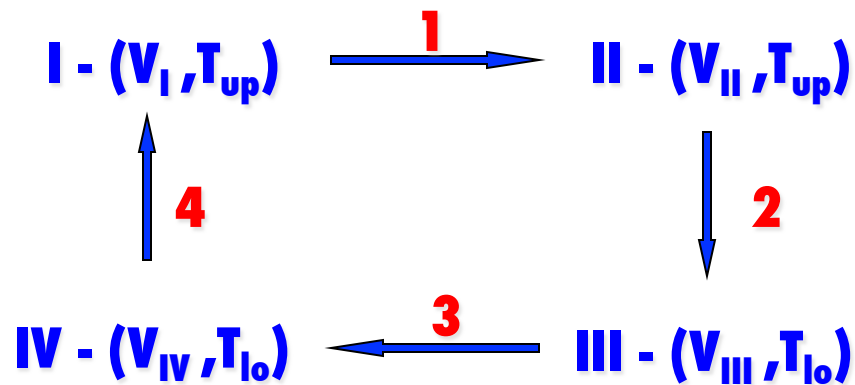
1,3 - Reversible and isothermal processes

2,4 - Reversible and adiabatic processes

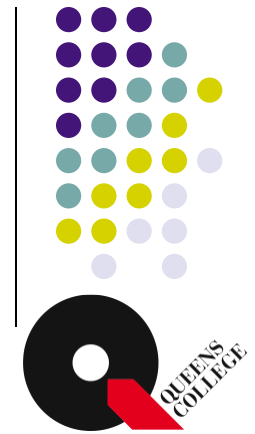
$$\Delta S_1 = nR \ln \left(\frac{V_{II}}{V_I} \right) \quad \text{and} \quad \Delta S_3 = nR \ln \left(\frac{V_{IV}}{V_{III}} \right)$$

$$\Delta S_2 = \Delta S_4 = 0$$

Carnot Cycle (Ideal Gas)



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1,3 - Reversible and isothermal processes

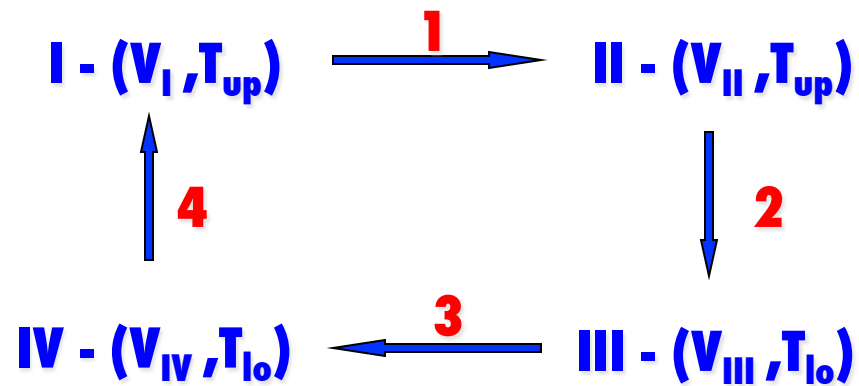
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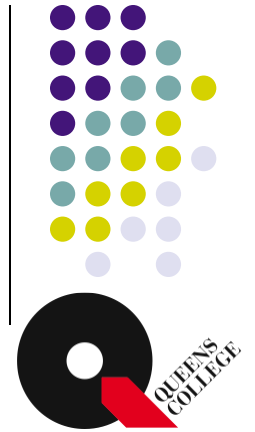
$$\Delta S = \Delta S_1 + \Delta S_2 + \Delta S_3 + \Delta S_4 = nR \ln \left(\frac{V_{II} V_{IV}}{V_I V_{III}} \right)$$

Carnot Cycle (Ideal Gas)

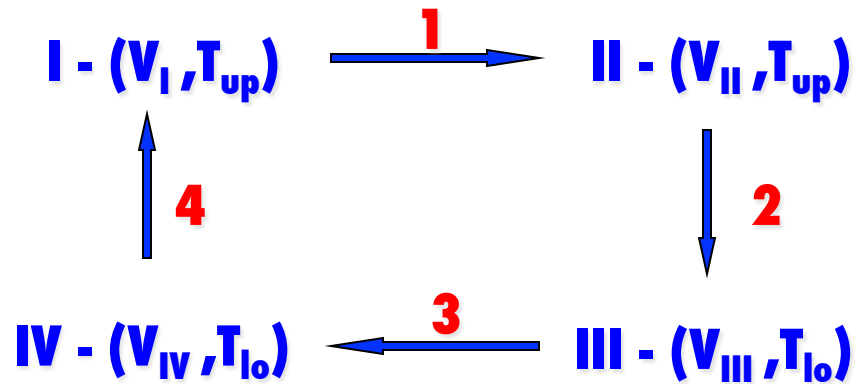


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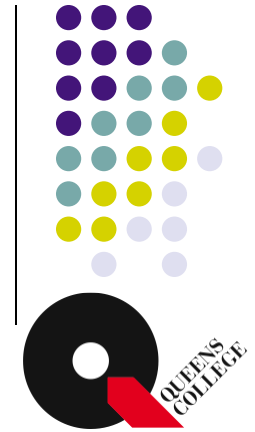
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Carnot Cycle (Ideal Gas)



**Fig. 3.6 (with
different notations)**



$$\Delta S = \Delta S_1 + \Delta S_2 + \Delta S_3 + \Delta S_4 = nR \ln \left(\frac{V_{II} V_{IV}}{V_I V_{III}} \right)$$

$$\frac{V_{II}}{V_{III}} = \left(\frac{T_{lo}}{T_{up}} \right)^c \quad \text{and} \quad \frac{V_{IV}}{V_I} = \left(\frac{T_{up}}{T_{lo}} \right)^c, \quad \text{where} \quad c = \frac{C_V}{nR}$$

See further information 2.1 (page 69)

Carnot Cycle (Ideal Gas)

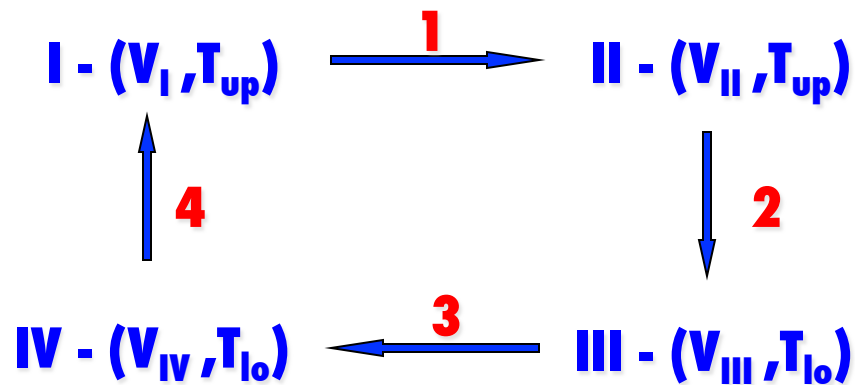
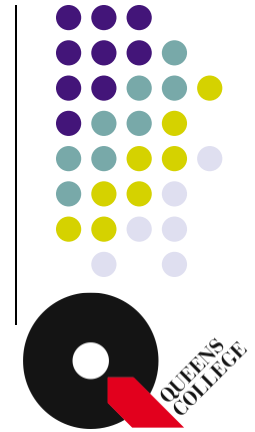


Fig. 3.6 (with different notations)



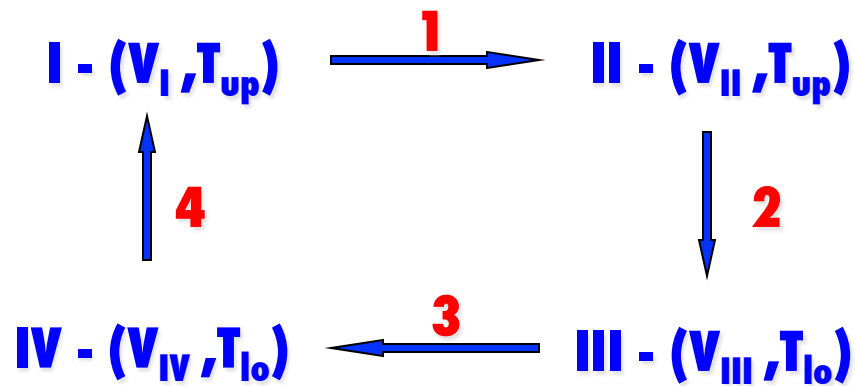
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See further information 2.1 (page 69)

$$\longrightarrow \Delta S = nR \ln \left(\frac{T_{lo} T_{up}}{T_{up} T_{lo}} \right)^c = nR \ln 1 = 0$$

Carnot Cycle (Ideal Gas)



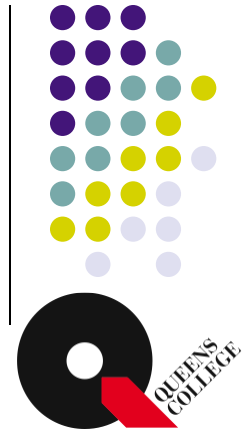
$$1 : q_1 = q_{up}, w_1 = -q_{up}$$

$$2 : q_2 = 0, w_2 = -w_{ad}$$

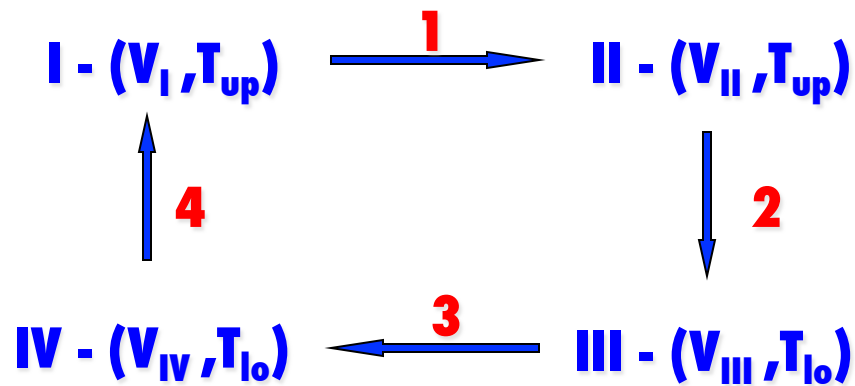
$$3 : q_3 = -q_{lo}, w_3 = q_{lo}$$

$$4 : q_4 = 0, w_4 = w_{ad}$$

$$\Delta S = 0 = S_1 + S_3 = \frac{q_{up}}{T_{up}} - \frac{q_{lo}}{T_{lo}} \longrightarrow \frac{q_{up}}{q_{lo}} = \frac{T_{up}}{T_{lo}}$$



Carnot Cycle (Ideal Gas)



$$1 : q_1 = q_{up}, w_1 = -q_{up}$$

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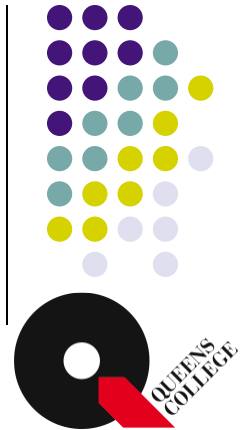
$$3 : q_3 = -q_{lo}, w_3 = q_{lo}$$

$$4 : q_4 = 0, w_4 = w_{ad}$$

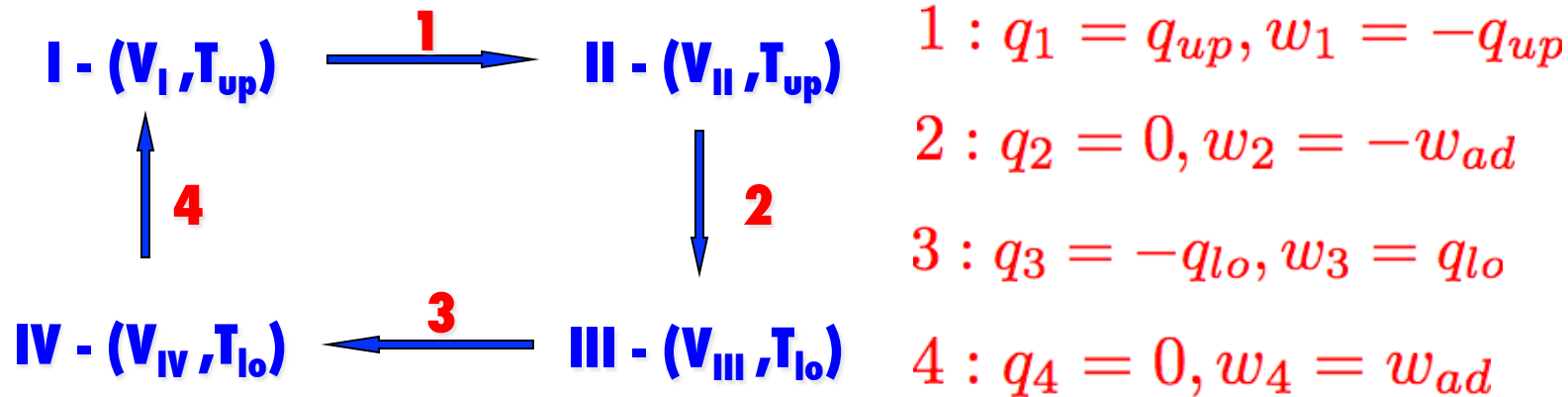
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$$q = q_{up} - q_{lo}$$

$$w = w_1 + w_2 + w_3 + w_4 = -q_{up} + q_{lo} = -q$$



Carnot Cycle (Ideal Gas)

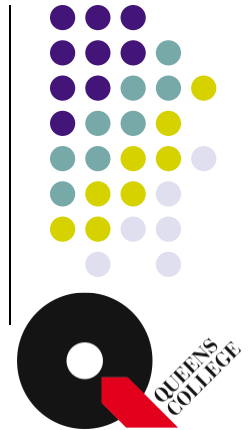


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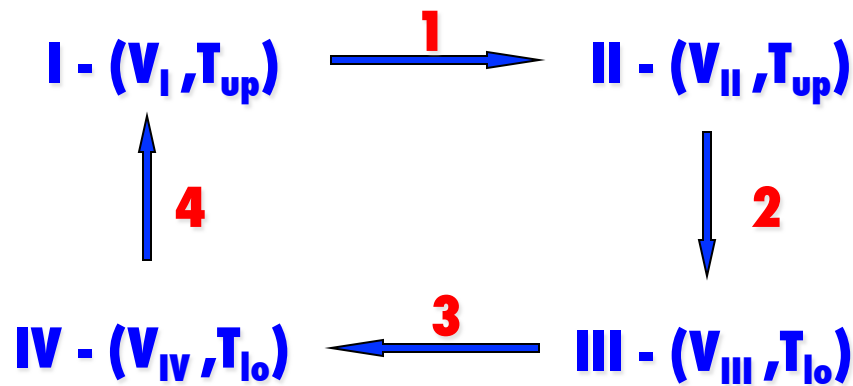
$$q = q_{up} - q_{lo}$$

$$w = w_1 + w_2 + w_3 + w_4 = -q_{up} + q_{lo} = -q$$

Efficiency: $\mathcal{E} = \frac{-w}{q_{up}} = \frac{q_{up} - q_{lo}}{q_{up}} = 1 - \frac{q_{lo}}{q_{up}} = 1 - \frac{T_{lo}}{T_{up}}$



Carnot Cycle (General)



$$1 : q_1 = q_{up}$$

$$2 : q_2 = 0$$

$$3 : q_3 = -q_{lo}$$

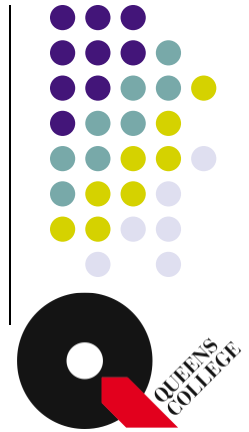
$$4 : q_4 = 0$$

$$\Delta S = S_1 + S_3 = \frac{q_{up}}{T_{up}} - \frac{q_{lo}}{T_{lo}}$$

$$q = q_{up} - q_{lo} \longrightarrow w = -q \quad \text{(First law)}$$

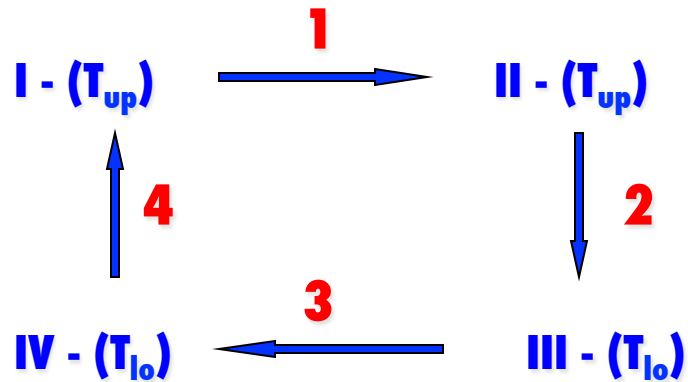
Efficiency: $\mathcal{E} = -\frac{w}{q_{up}} = \frac{q_{up} - q_{lo}}{q_{up}} = 1 - \frac{q_{lo}}{q_{up}} = ?$

If $\mathcal{E} \neq 1 - \frac{T_{lo}}{T_{up}} = \mathcal{E}_{id}$, then $\Delta S \neq 0 \longrightarrow \mathbf{S}$ is not a state function

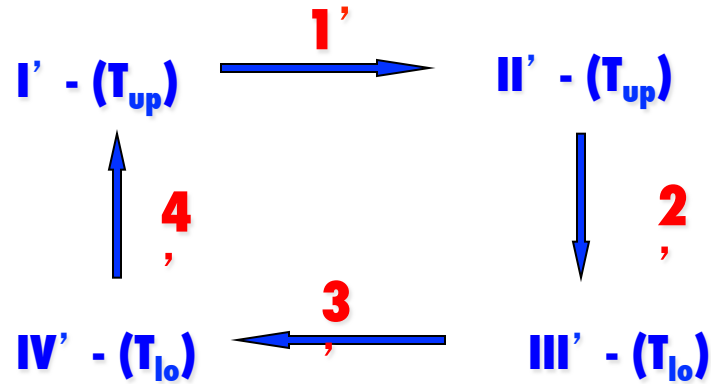


Proof that $\mathcal{E} = \mathcal{E}_{id}$

Carnot cycle A with \mathcal{E}

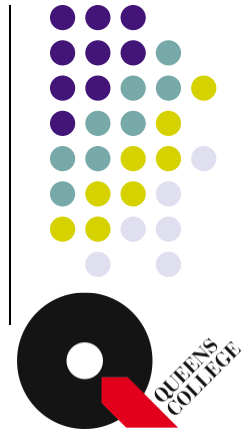


Carnot cycle B with \mathcal{E}'

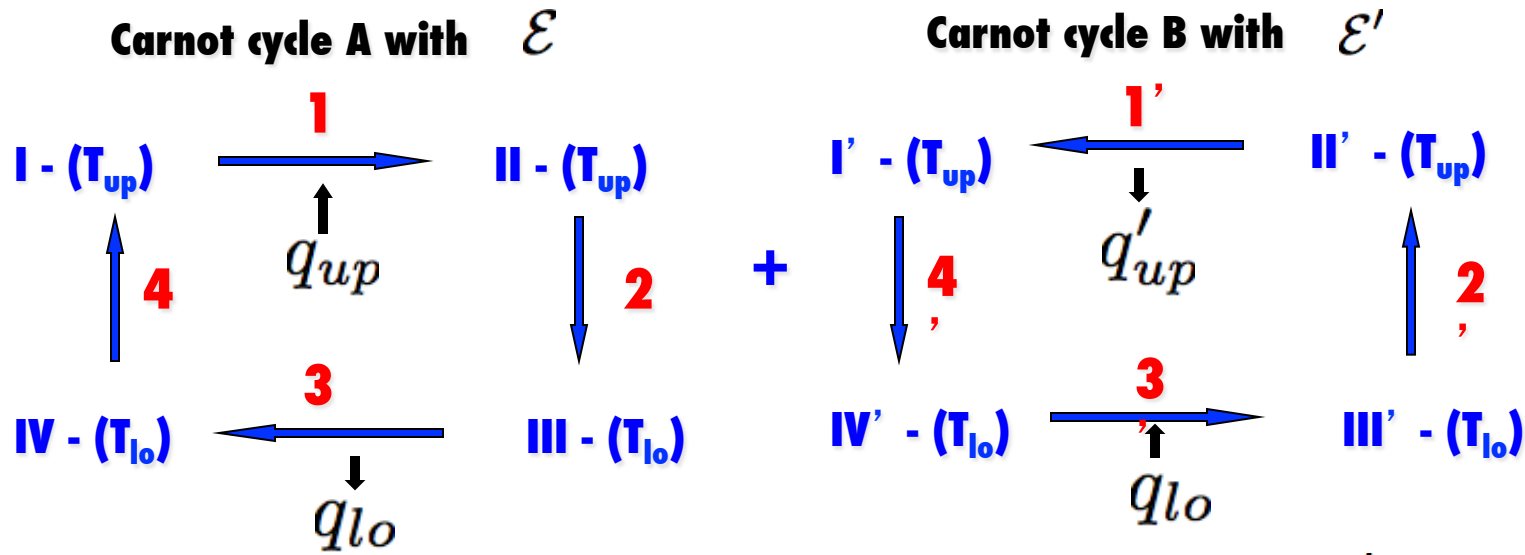
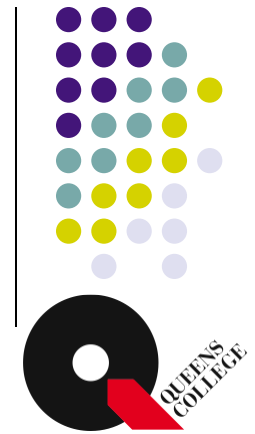


Assume that $\mathcal{E} > \mathcal{E}'$

Then, $1 - \frac{q_{lo}}{q_{up}} > 1 - \frac{q'_{lo}}{q'_{up}}$



Proof that $\mathcal{E} = \mathcal{E}_{id}$



Assume that $\mathcal{E} > \mathcal{E}'$

Then, $1 - \frac{q_{lo}}{q_{up}} > 1 - \frac{q'_{lo}}{q'_{up}}$

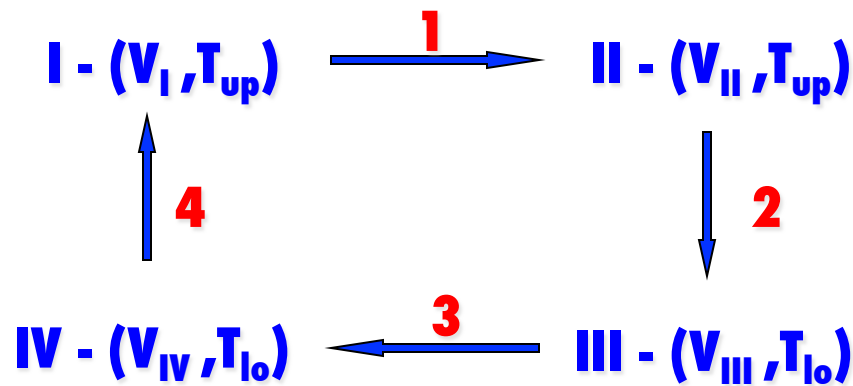
Combine A and reverse of B, and assume $q_{lo} = q'_{lo}$

Then, $q_{up} > q'_{up} \longrightarrow w - w' = -q_{up} + q'_{up} < 0$

Complete conversion of heat $q_{up} - q'_{up}$ into work $-w + w'$

This contradicts the second law by Kelvin! $\longrightarrow \mathcal{E} = \mathcal{E}'$

Carnot Cycle (General)



$$1 : q_1 = q_{up}$$

$$2 : q_2 = 0$$

$$3 : q_3 = -q_{lo}$$

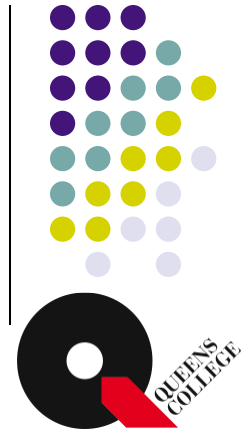
$$4 : q_4 = 0$$

Efficiency:
$$\mathcal{E} = -\frac{w}{q_{up}} = \frac{q_{up} - q_{lo}}{q_{up}} = 1 - \frac{q_{lo}}{q_{up}} = \mathcal{E}_{id} = 1 - \frac{T_{lo}}{T_{up}}$$

$$\Delta S = S_1 + S_3 = \frac{q_{up}}{T_{up}} - \frac{q_{lo}}{T_{lo}} = \frac{q_{up}}{T_{lo}} \left(\frac{T_{lo}}{T_{up}} - \frac{q_{lo}}{q_{up}} \right) = 0$$

Any cycle can be considered as the sum of infinitesimal Carnot cycles (Fig. 3.9) $\longrightarrow \oint \frac{dq_{rev}}{T} = \sum_{Carnot,i} \Delta S_i = 0$

S defined such that $dS = \frac{dq_{rev}}{T}$ is a state function.



Clausius Inequality: $dS \geq \frac{dq}{T}$



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(i) $-dW_{rev} \geq -dW$

System does maximum work for reversible process.

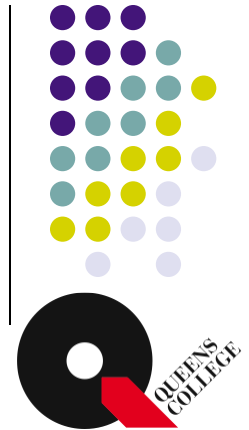
(ii)

Consider a change of system through a reversible process

$$dU = dq_{rev} + dW_{rev} \quad (1)$$

The same change can happen through another process.

$$dU = dq + dW \quad (2)$$



Clausius Inequality: $dS \geq \frac{dq}{T}$

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Consider a change of system through a reversible process

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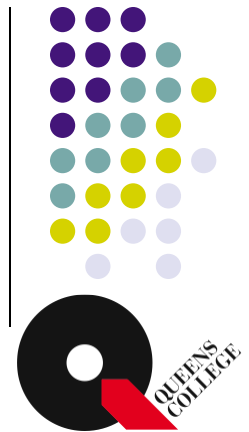
$$(1)=(2) \longrightarrow dq_{rev} + dW_{rev} = dq + dW$$

$$\longrightarrow TdS - dq = dW - dW_{rev} \geq 0$$

↑

(i)

For adiabatic process $dS \geq 0$



Entropy change due to phase transition

Normal transition temperature: temperature at which two phases are in equilibrium at 1 atm.

Heat transfer during phase transition is reversible

$$\Delta_{trs}S = \frac{\Delta q}{T_{trs}} = \frac{\Delta_{trs}H}{T_{trs}}$$

Constant pressure

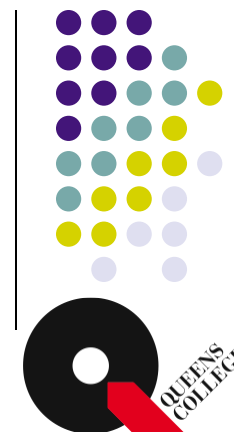
Entropy change due to heating

$$S(T_f) - S(T_i) = \int_{T_i}^{T_f} \frac{dq_{rev}}{T} = \int_{T_i}^{T_f} \frac{C_p dT}{T}$$

Constant pressure

If C_p is independent of temperature

$$= C_p \ln \left(\frac{T_f}{T_i} \right)$$



Entropy of a gas

$$S(T) = S(0) + \int_0^{T_f} \frac{C_p(s)}{T} dT + \frac{\Delta_{fus}H}{T_f} + \int_{T_f}^{T_b} \frac{C_p(l)}{T} dT \\ + \frac{\Delta_{vap}H}{T_b} + \int_{T_b}^T \frac{C_p(g)}{T} dT$$

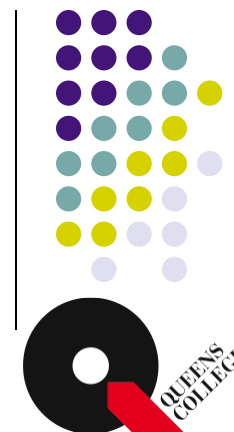
$$C_p(s) \propto T^3 \text{ as } T \rightarrow 0 \quad \text{(Debye extrapolation)}$$

Nernst heat theorem

$\Delta S \rightarrow 0$ as $\Delta T \rightarrow 0$ for perfect crystalline substances

Third law of thermodynamics

For perfect crystalline substances, $S = 0$ at $T = 0$.



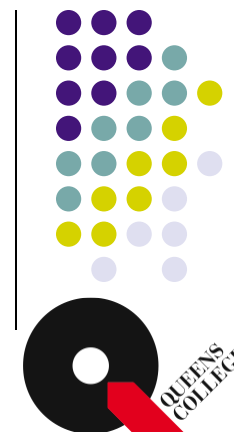
Standard (third law) entropy

$S^\ominus(T)$ - the entropy in the standard state under the assumption that $S=0$ at $T=0$.

Entropy of reaction for $\sum_i \nu_i M_i \rightarrow \sum_f \nu_f M_f$

$$\Delta_r S^\ominus = \sum_f \nu_f S_m^\ominus(f) - \sum_i \nu_i S_m^\ominus(i)$$

Standard of entropies of ions are defined such that $S^\ominus(H^+, \text{aq}) = 0$



Helmholtz free energy

**Determines the spontaneous
(free) process at constant volume**

$$A = U - TS$$

$$dS \geq \frac{dq}{T} \longrightarrow (dA)_{T,V} = dq - TdS \leq 0$$

(no non-expansion work)

Gibbs free energy

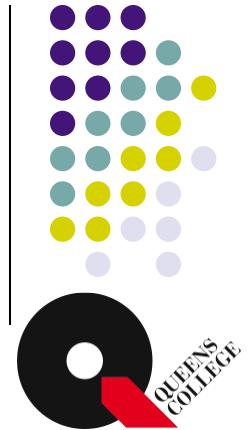
**Determines the spontaneous
(free) process at constant process**

$$G = H - TS = U + pV - TS$$

$$dS \geq \frac{dq}{T} \longrightarrow (dG)_{T,p} = dq - TdS \leq 0$$

(no non-expansion work)

$$(dG)_{T,p} = (dU)_{T,p} + pdV - TdS = dq - pdV + pdV - TdS$$



Helmholtz free energy

**Determines the spontaneous
(free) process at constant volume**

$$A = U - TS$$

$$dS \geq \frac{dq}{T} \longrightarrow (dA)_{T,V} = dq - TdS \leq 0$$

(no non-expansion work)

$$\underline{-(dA)_T = -dW - dq + TdS \geq -dW}$$

Maximum work system can do in isothermal situation

Gibbs free energy

**Determines the spontaneous
(free) process at constant process**

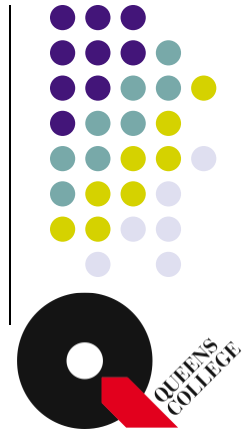
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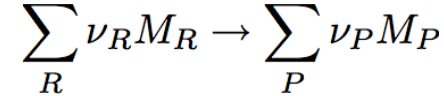
(no non-expansion work)

$$\underline{-(dG)_{T,P} = -dq + pdV - dW_e - pdV + TdS \geq -dW_e}$$

**Maximum non-expansion work system can do in
isothermal and isobaric situation**



Standard Gibbs energy of reaction



$$\Delta_r G^\ominus = \sum_P \nu_P \Delta_f G_P^\ominus - \sum_R \nu_R \Delta_f G_R^\ominus$$

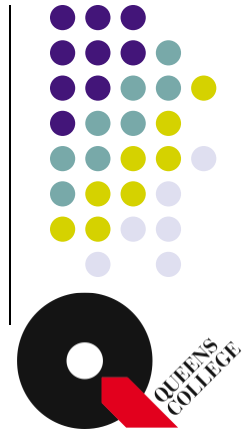


Standard Gibbs energy of formation

The standard Gibbs energy of formation for ions are defined such that

$$\Delta_f G^\ominus(H^+, \text{aq}) = 0$$

zero standard Gibbs energy of formation at all temperature



Fundamental equation

closed system, no non-expansion work, reversible change

$$dU = dq_{rev} + dW_{rev,exp} = \frac{TdS - pdV}{\uparrow}$$

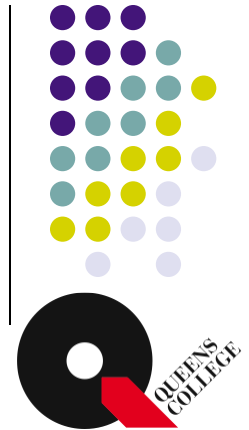
valid even for irreversible change

Assume $U = U(S, V) \longrightarrow dU = \left(\frac{\partial U}{\partial S}\right)_V dS + \left(\frac{\partial U}{\partial V}\right)_S dV$

$$\left(\frac{\partial U}{\partial S}\right)_V = T \quad \text{and} \quad \left(\frac{\partial U}{\partial V}\right)_S = -p$$

Assume that $T = T(S, V)$ and $p = p(S, V)$

$$\left(\frac{\partial T}{\partial V}\right)_S = \frac{\partial^2 U}{\partial V \partial S} = \frac{\partial^2 U}{\partial S \partial V} = - \left(\frac{\partial p}{\partial S}\right)_V$$



$$dA = d(U - TS) = TdS - pdV - TdS - SdT = -SdT - pdV$$

$$dH = d(U + pV) = TdS - pdV + pdV + Vdp = TdS + Vdp$$

$$dG = d(H - TS) = TdS + Vdp - TdS - SdT = -SdT + Vdp$$



$$dA = d(U - TS) = TdS - pdV - TdS - SdT = -SdT - pdV \quad \mathbf{(2)}$$

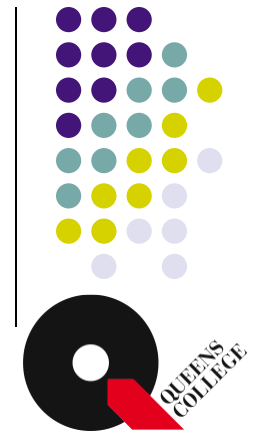
$$dH = d(U + pV) = TdS - pdV + pdV + Vdp = TdS + Vdp \quad \mathbf{(3)}$$

$$dG = d(H - TS) = TdS + Vdp - TdS - SdT = -SdT + Vdp \quad \mathbf{(4)}$$

$$\left(\frac{\partial A}{\partial T}\right)_V = -S, \left(\frac{\partial A}{\partial V}\right)_T = -p \quad \mathbf{(2')}$$

$$\left(\frac{\partial H}{\partial S}\right)_p = T, \left(\frac{\partial H}{\partial p}\right)_S = V \quad \mathbf{(3')}$$

$$\left(\frac{\partial G}{\partial p}\right)_T = V, \left(\frac{\partial G}{\partial T}\right)_p = -S \quad \mathbf{(4')}$$



$$dA = d(U - TS) = TdS - pdV - TdS - SdT = -SdT - pdV \quad \mathbf{(2)}$$

$$dH = d(U + pV) = TdS - pdV + pdV + Vdp = TdS + Vdp \quad \mathbf{(3)}$$

$$dG = d(H - TS) = TdS + Vdp - TdS - SdT = -SdT + Vdp \quad \mathbf{(4)}$$

$$\left(\frac{\partial A}{\partial T}\right)_V = -S, \quad \left(\frac{\partial A}{\partial V}\right)_T = -p \quad \mathbf{(2')}$$

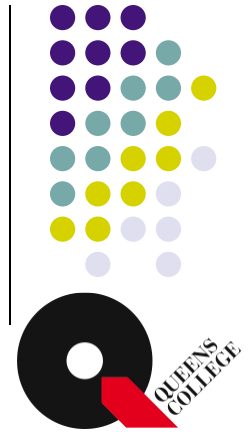
$$\left(\frac{\partial H}{\partial S}\right)_p = T, \quad \left(\frac{\partial H}{\partial p}\right)_S = V \quad \mathbf{(3')}$$

$$\left(\frac{\partial G}{\partial p}\right)_T = V, \quad \left(\frac{\partial G}{\partial T}\right)_p = -S \quad \mathbf{(4')}$$

$$\mathbf{(2')} \rightarrow \left(\frac{\partial S}{\partial V}\right)_T = \left(\frac{\partial p}{\partial T}\right)_V \quad \frac{\partial^2 A}{\partial T \partial V} = \frac{\partial^2 A}{\partial V \partial T}$$

$$\mathbf{(3')} \rightarrow \left(\frac{\partial T}{\partial p}\right)_S = \left(\frac{\partial V}{\partial S}\right)_p \quad \frac{\partial^2 H}{\partial p \partial S} = \frac{\partial^2 H}{\partial S \partial p}$$

$$\mathbf{(4')} \rightarrow \left(\frac{\partial V}{\partial T}\right)_p = -\left(\frac{\partial S}{\partial p}\right)_T \quad \frac{\partial^2 G}{\partial T \partial p} = \frac{\partial^2 G}{\partial p \partial T}$$



Gibbs-Helmholtz equation

$$G = H - TS$$

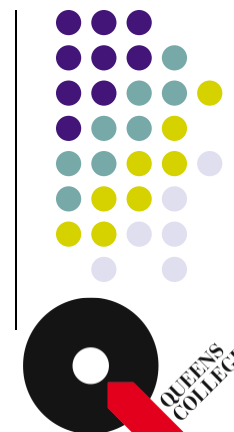
$$\rightarrow \frac{H - G}{T} = S = - \left(\frac{\partial G}{\partial T} \right)_p$$

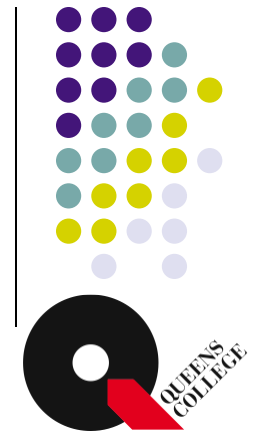
$$\rightarrow \frac{1}{T} \left(\frac{\partial G}{\partial T} \right)_p - \frac{G}{T^2} = - \frac{H}{T^2}$$

$$\rightarrow \frac{\partial}{\partial T} \left(\frac{G}{T} \right)_p = - \frac{H}{T^2}$$

$$\rightarrow \frac{\partial}{\partial T} \left(\frac{\Delta G}{T} \right)_p = - \frac{\Delta H}{T^2}$$

**Important equation for
understanding phase transition**





At constant temperature,

$$dG = V dp$$

$$\longrightarrow G_m(p_f) = G_m(p_i) + \int_{p_i}^{p_f} V_m dp$$

\uparrow \uparrow \uparrow

Molar Gibbs energy **Molar volume**

For liquids or solids, V_m is insensitive to pressure change

$$G_m(p_f) \approx G_m(p_i) + V_m \int_{p_i}^{p_f} dp = G_m(p_i) + (p_f - p_i)V_m$$

For an ideal gas,

$$G_m(p_f) = G_m(p_i) + \int_{p_i}^{p_f} \frac{RT}{p} dp = G_m(p_i) + RT \ln \left(\frac{p_f}{p_i} \right)$$

$$G_m(p) = G_m^\ominus + RT \ln \left(\frac{p}{p^\ominus} \right) \quad \text{When } p_i = p^\ominus$$